

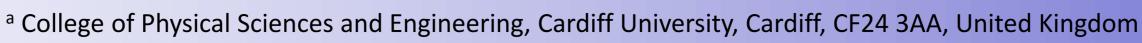
EÖTVÖS LORÁND



# for the oxidation of NH<sub>3</sub>/H<sub>2</sub> mixtures Ali Alnasif<sup>a,b</sup>, Joanna Jójka<sup>c</sup>, Máté Papp<sup>d</sup>, András György Szanthoffer<sup>d,e</sup>, Marina Kovaleva<sup>a</sup>,

Tamás Turányi<sup>d</sup>, Syed Mashruk<sup>a</sup>, Agustin Valera-Medina<sup>a,\*</sup>, Tibor Nagy<sup>f,\*</sup>

A compact kinetic reaction mechanism



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1.63

2.70

3.06

3.21

3.41

3.51

3.67

3.85

3.91

4.01

4.74

4.79

5.17

6.21

6.22

6.29

6.68

6.76

NH<sub>3</sub> H<sub>2</sub> O<sub>2</sub> H<sub>2</sub>O N<sub>2</sub> NO N<sub>2</sub>O NH<sub>3</sub> H<sub>2</sub> O<sub>2</sub> H<sub>2</sub>O NO NO<sub>2</sub> N<sub>2</sub>O

Zhu 2024 2.1 0.8 0.8 1.4 0.6 0.4 0.5 0.9 0.9 1.3 1.9 0.7 1.5 5.2

Han 2023 2.5 0.8 0.6 1.3 0.9 0.7 2.8 1.1 5.4 0.7 3.9 6.3 3.0 1.0

Jian 2024 | 2.2 | 2.6 | 1.0 | 1.3 | 2.8 | 0.5 | 0.5 | 1.8 | 5.1 | 0.7 | 4.0 | 2.8 | 2.2 | 6.5

Present work 4.0 2.3 2.9 3.3 2.7 1.3 1.5 0.7 5.6 0.8 3.9 1.5 3.6 3.2

Otomo 2018 | 2.9 | 1.4 | 2.5 | 2.3 | 2.4 | 0.5 | 1.0 | 0.8 | 5.3 | 0.8 | 3.8 | 5.4 | 1.9 | 4.1

Stagni 2023 | 2.0 1.3 0.8 1.8 2.1 0.6 2.7 | 1.5 5.4 0.7 4.0 3.3 2.7 9.4

Stagni 2020 | 2.0 1.3 0.5 1.6 1.5 0.7 8.1 | 1.1 5.7 0.7 3.8 7.2 2.8 7.6

Glarborg 2022 3.1 2.4 1.2 2.8 3.2 1.4 2.9 2.1 5.3 0.8 4.1 1.8 2.2 9.0

Glarborg 2023 3.1 2.4 1.2 2.8 3.2 1.4 2.9 2.2 5.3 0.8 4.0 1.8 2.2 9.0

Z. Zhang 2024 | 2.1 0.6 1.1 1.5 0.6 0.5 0.4 | 3.1 4.1 0.7 4.0 2.9 2.4 9.2

Tamaoki 2024 | 2.9 | 1.2 | 2.3 | 1.8 | 2.3 | 1.8 | 2.3 | 17.2 | 8.2 | 9.3 | 10.8 | 5.7 | 3.8 | 10.5

Glarborg 2018 | 4.1 | 2.4 | 1.6 | 4.1 | 3.6 | 1.3 | 2.8 | 2.9 | 5.1 | 0.8 | 4.1 | 2.9 | 2.2 | 9.6

San Diego 2018 | 2.8 | 3.1 | 1.1 | 3.1 | 1.0 | 0.7 | 3.4 | 24.9 | 10.1 | 12.3 | 15.8 | 9.7 | 5.5 | 10.

20 Klippenstein 2018 | 4.1 | 2.4 | 1.6 | 4.1 | 3.6 | 1.3 | 2.8 | 2.9 | 5.1 | 0.8 | 4.2 | 2.9 | 2.2 | 9.6

Liu 2024 2.7 1.4 1.4 2.7 1.1 1.2 4.3 1.5 5.5 0.7 3.9 6.2 3.2 9.6

He 2023 3.2 2.7 1.1 2.7 3.1 1.0 2.4 2.9 4.1 0.8 3.9 2.5 2.3 9.3

Mei 2021 | 2.3 1.7 2.0 1.6 1.8 0.6 0.8 | 17.1 6.1 9.4 10.4 1.8 3.6 11.6

Wang 2022 3.6 3.5 2.7 3.0 2.0 1.5 0.9 17.2 8.2 9.3 10.9 5.1 3.8 10.5

Meng 2023 | 4.1 | 2.4 | 1.6 | 4.1 | 3.6 | 1.3 | 3.4 | 2.9 | 5.1 | 0.8 | 4.1 | 2.5 | 2.4 | 9.3

1500

· Present work

measurement limit

Equivalence ratio

Equivalence ratio

···· • ···· Exp. Mashruk 2023

Gotama 2022 | 2.9 | 3.7 | 2.1 | 2.4 | 1.2 | 1.2 | 5.0 | 1.0 | 5.6 | 0.7 | 3.8 | 5.1 | 3.1 | 8.1

Nakamura 2019 | 3.9 | 3.6 | 0.9 | 4.2 | 3.0 | 0.6 | 1.4 | 2.7 | 5.3 | 0.7 | 4.0 | 2.7 | 2.7 | 9.4

X. Zhang 2021 3.5 2.8 1.3 3.1 3.5 1.1 3.0 1.3 5.6 0.7 3.8 3.9 2.8 8.7

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Mechanism  $N_{\text{spec}}N_{\text{reac}}\sqrt{E_{\text{LBV}}}\sqrt{E_{\text{JSR}}}\sqrt{E_{\text{BSSF}}}\sqrt{E_{\text{Overall}}}$ 

Zhu 2024 39 312 2.97

Han 2023 32 171 2.24

Jian 2024 32 233 3.23

**Present work** 21 64 1.97

Otomo 2018 32 213 3.67

Stagni 2023 31 203 3.46

Stagni 2020 31 203 3.32

Glarborg 2023 34 228 6.52 2.54

32 165 3.28

Liu 2024 35 238 3.96 2.39

**Z. Zhang 2024** 34 224 8.46 1.14 4.50

Tamaoki 2024 33 228 3.29 2.14 10.17

Meng 2023 39 269 10.14 3.11 4.62

Wang 2022 32 140 2.53 2.64

34 227 6.42 2.55

He 2023 34 221 7.37 2.46 4.45

Mei 2021 35 239 4.02 1.65 9.84

X. Zhang 2021 34 224 2.45

Nakamura 2019 34 229 3.75

20 Klippenstein 2018 33 108 10.28 3.03

Glarborg 2018 33 211 10.29 3.03

22 San Diego 2018 21 64 3.36 2.43 13.94

Gotama 2022

Glarborg 2022

Mechanism

**2500** 

<u>e</u> 2000

1000

500

1500

Equivalence ratio

··· • ··· Exp. Mashruk 2023











Laboratory **ELTE** 

- In this poster we present the development and validation of our recently proposed compact NH<sub>3</sub> reaction mechanism [1].
- The potential of ammonia as a zero-carbon fuel and hydrogen carrier has stimulated scientific interest in its application as a fuel in combustion systems.
- However, the use of ammonia as a fuel source for energy applications presents notable challenges due to its low flammability and the potential for high emissions [2].
- Blending NH<sub>3</sub> with H<sub>2</sub> offers the prospect of improving combustibility, albeit with a notable increase in NOx emissions, especially under fuel-rich conditions [3].
- The design of burners, turbines, and engines is aided by computational fluid dynamics (CFD) simulations, which require small-sized mechanisms.
- According to a recent review of the performance of ammonia combustion mechanisms [4], the San Diego 2018 mechanism [5], which has an exceptionally small size (21 species, 64 reactions), shows fair performance in predicting laminar burning velocities (LBV) and concentration data measured in jet-stirred reactors (JSR) under a wide range of conditions.
- The current study aims to develop a small and robust kinetic mechanism for CFD simulations of NH<sub>3</sub>/H<sub>2</sub> flames by optimising the rate parameters of the San Diego 2018 NH<sub>3</sub> mechanism against experimental data using the Optima++ code [6-8].

## **Experimental Data Collection**

- A large collection of LBV and concentration data measured in JSRs, previously compiled from the literature [4] was downloaded in ReSpecTh Kinetic Data (RKD) format XML files [9] from the Reaction Kinetic branch **ReSpecTh database** [10-11].
- burneraddition, **concentration** data from stabilised stagnation flames (BSSF) [12], recently published LBV data were collected.
- All newly collected data were coded in RKD files [9] and will be available in the **ReSpecTh database** [10-11].
- See ECM manuscript for corresponding publications.

points	mixture (%)	(atm)	range (K)	ratio $(\varphi)$
1283	0-100	1.0–36.6	295-584	0.2–2.0
538	10-70	1	800–1300	0.15-1.5
119	30	1	298	0.57–1.4
1968	0-100	0.5-10	295-1300	0.15-2.0
	538 119	1283 0-100 538 10-70 119 <b>30</b>	1283     0-100     1.0–36.6       538     10-70     1       119     30     1	1283     0-100     1.0-36.6     295-584       538     10-70     1     800-1300       119     30     1     298

## **Optimization method**

• The Optima++ code with the FOCTOPUS algorithm [6-8] minimizes the following error function:

$$\boldsymbol{E}(\mathbf{P}) = \frac{1}{N} \sum_{f=1}^{N_f} \sum_{s=1}^{N_{fsd}} \frac{w_{fsd}}{N_{fsd}} \sum_{d=1}^{N_{fsd}} \left( \frac{Y_{fsd}^{sim}(\mathbf{P}) - Y_{fsd}^{exp,tot}}{\sigma_{fsd}^{exp,tot}} \right)^2$$

$$f,s,d: \text{ data file index, data series index, data}$$

$$f,s,d: \text{ data file index, data series index, data}$$

$$f,s,d: \text{ data file index, data series sin data file } f$$

$$f,s,d: \text{ data series sin data file } f$$

- points index P: vector of model parameters
- the total number of the data series
- $N_{f/s/d}$ : the number of the data files/series/points
- data series s in data file f weigths to equalize an data collection which may contain different number of data series of each experiment type.
- $\sqrt{E}$  measures the RMS deviation between the model and the experimental results, with respect to  $\sigma^{\text{exp}}$ . A mechanism is typically considered accurate if  $\sqrt{E}$  < 3.
- Weights to balance the contribution of different experimental types: (LBV: 1/179, JSR: 1/47, BSSF:1/7)
- Sensitivity analysis found all the 64 rate coefficients important.
- The initial model missing important chemistry, which can be compensated by unphysical rate coefficients.
- Thus, one order of magnitude prior uncertainty range was employed for parameter tuning.
- For the simulations, we used Cantera 2.6 [13].

# Results

- The performance of the initial and optimized San Diego 2018 models were compared with 19 recent models (refs→ECM paper).
- Significantly improved accuracy of the optimised mechanism (present work, PW) vs. the San Diego 2018 (SD) model in predicting the LBVs ( $\sqrt{E}$ : 3.36 $\rightarrow$ 1.97)
- PW is currently the most accurate model for LBV simulations with the shortest computational time.
- For BSSF simulations of 70/30 vol% NH<sub>3</sub>/H<sub>2</sub> mixtures, the accuracy of the model improved greatly ( $\sqrt{E}$ : 13.91 $\rightarrow$ 3.24).
- Except for Zhu 2024, all models perform poorly for BSSF data.
- The model performance for JSR concentrations (with at least 10% of H<sub>2</sub>) slightly deteriorated upon optimisation (2.43 $\rightarrow$ 2.72) but  $\sqrt{E}$ remained below 3.
  - The Zhu 2024 model shows outstanding performance for all species in JSR and BSSF simulations, except for NO<sub>2</sub> in BSSF.
  - The prediction for all species concentrations improved greatly upon optimization of the San Diego 2018 model in BSSF.
  - The PW model can accurately predict NO and N<sub>2</sub>O JSR data, but improvement is needed for other species, especially for NH<sub>3</sub> and H<sub>2</sub>O.
  - The PW model accurately predicts NO emissions and NH<sub>3</sub> slip in BSSF, while improvement is needed for  $H_2$ ,  $H_2O$  and  $NO_2$ .
  - Validation in Reynolds Averaged Navier Stokes (RANS) CFD simulations of a swirl burner against experimental data of **Mashruk et al.** [14]
  - All models predict N<sub>2</sub>O emission qualitatively well.
  - Stagni 2020 is the most accurate for NO peak conc.
  - Both the **Stagni 2020 and Nakamura 2019** models give qualitatively incorrect predictions at lean conditions: they fail to predict the very small NO emission, the nonzero NH<sub>3</sub> emission and the low NO<sub>2</sub> emission at  $\varphi$ =0.6.
  - The PW model predicts all four emissions qualitatively well over the whole  $\varphi$  range.
  - The PW model is the most computationally efficient , as it runs ~2 faster than the other two models.

#### **Concluding remarks**

- The accuracy of the San Diego 2018 mechanism could be greatly improved for laminar burning velocities and for concentrations in burner stabilized stagnation flames, and it is on par with best-performing mechanisms.
- However, its performance for concentrations in JSR, and for NO<sub>2</sub> concentration in BSSF need to be improved, which implies that the deficiencies in its chemistry cannot be compensated by the rates of other reaction routes.
- In CFD swirl burner simulations, it ran faster than other models and qualitatively captures all major emissions.

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